



Funding 2011

Biogas to Diesel



Funding 2016-Present



Winner 2010



U.S. DEPARTMENT OF ENERGY
ENERGY

Funding 2016-Present



Universities Addressing Florida's Energy Needs
Funding 2008



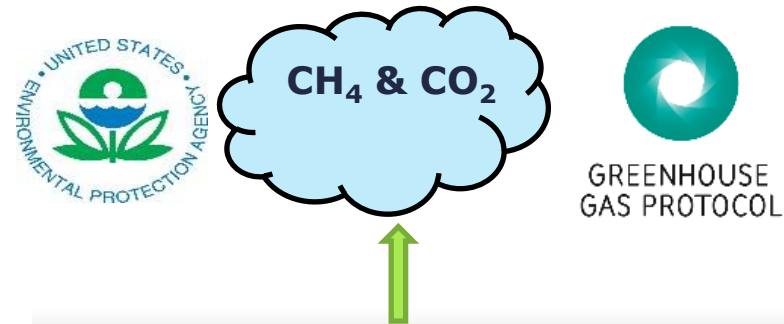
Innovation of the Year 2013



Funding 2014



30 Under 30 2014

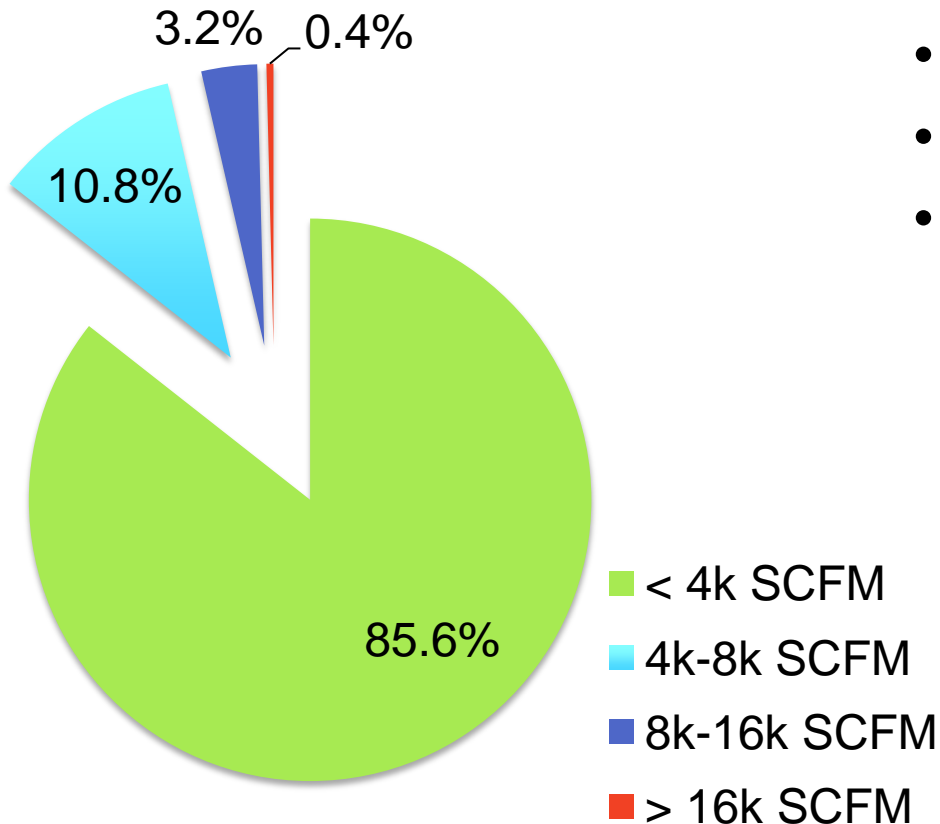


234 MM tons/year of Garbage

- 2,450 Landfills in US
- 20% of Human Source of Methane
- Requirement to Capture and Mitigate
- RFS Increase in RVO
- Waste Industry Consumes ~ 4% US Diesel consumption
- Ag Industry Consumes ~3% US Diesel Consumption
- AD Technology Advancements (~1,500 projects operating in US)

Total US Biogas Generation Rate ~ 800,000 SCFM

Landfill LFG Collection Rate



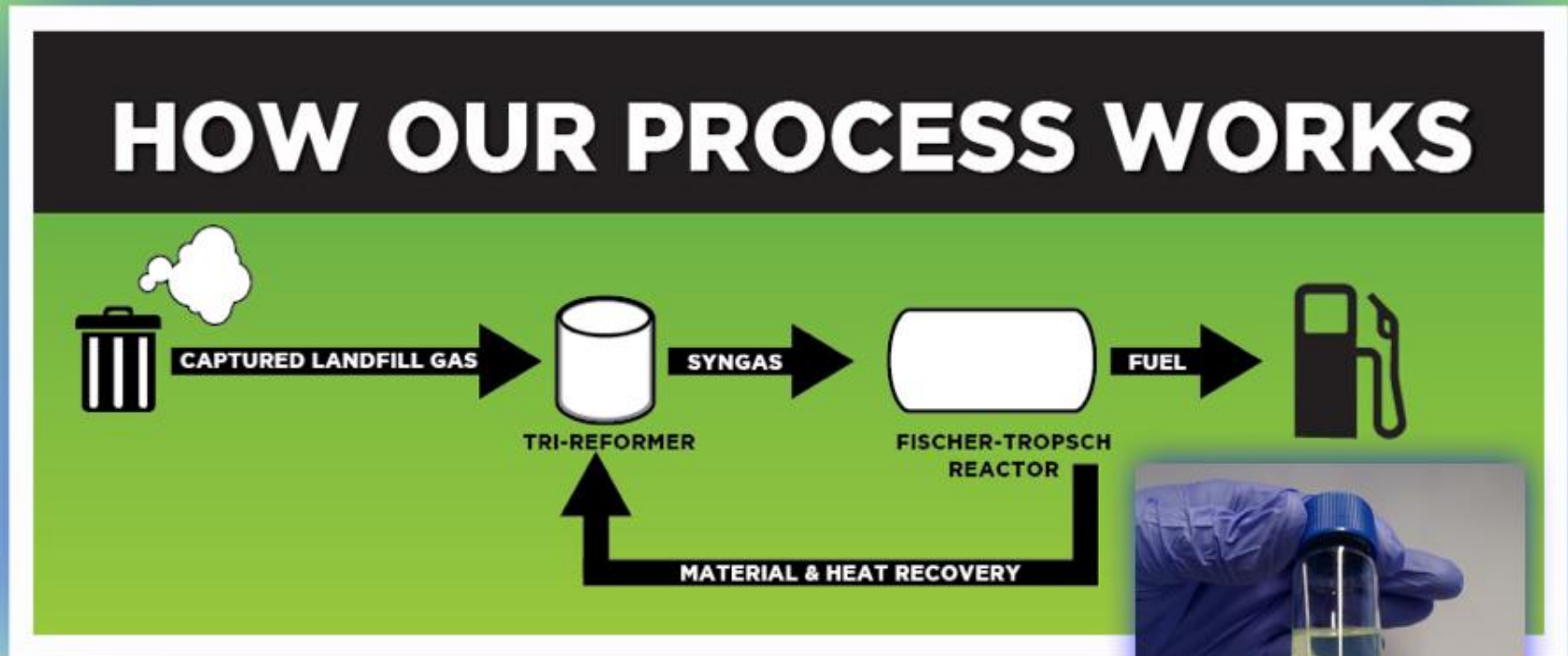
What's the best use of this energy resource?

- Electricity generation
- Biomethane
- Gas to Liquids

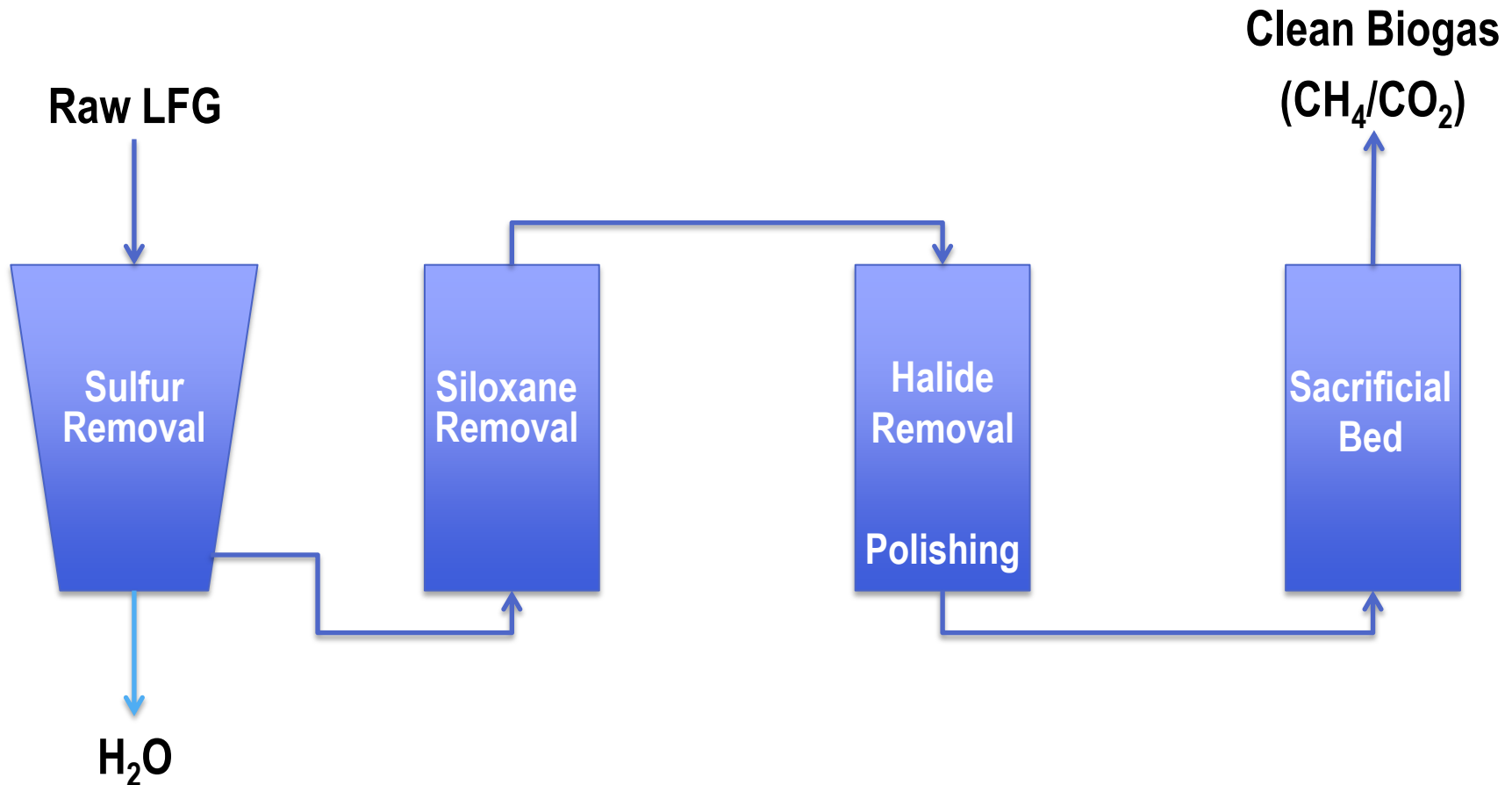
Key Factors

Economics
Infrastructure
Location
Efficiency
Policy

Demonstrate small scale GTL in economical and profitable manner

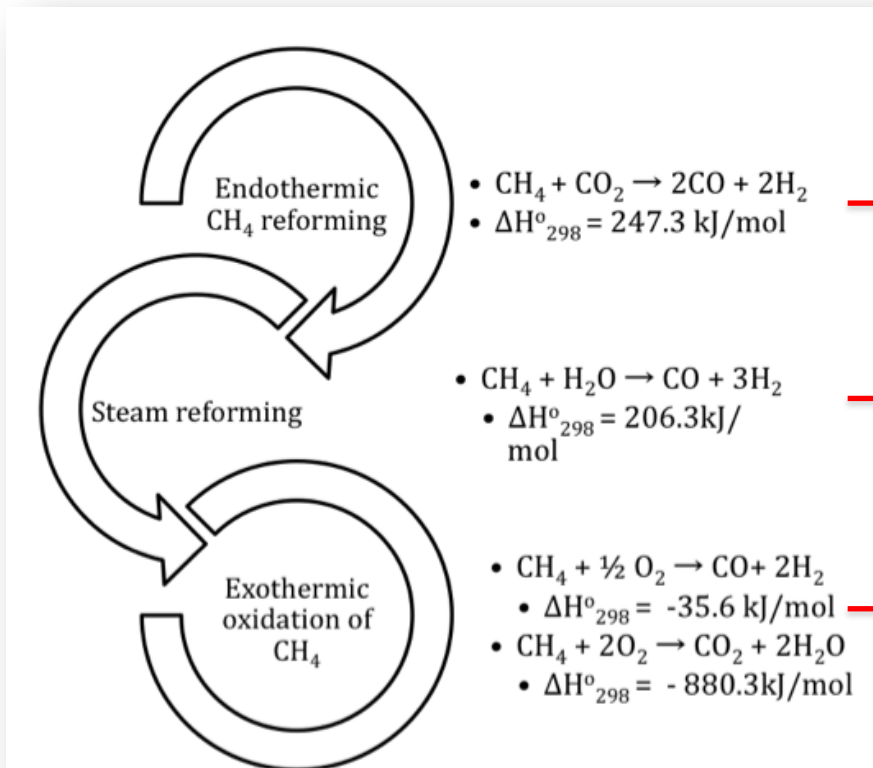


Trace Contaminant Pretreatment



Tri-reforming:

- Minimize cleanup and pretreatment process (No CO₂ removal)
- Less energy consumption
- Produce high quality syngas (H₂:CO ~ 2)



Utilize 100% of biogas as feedstock

Control H₂ and CO selectivity

Generate heat in-situ

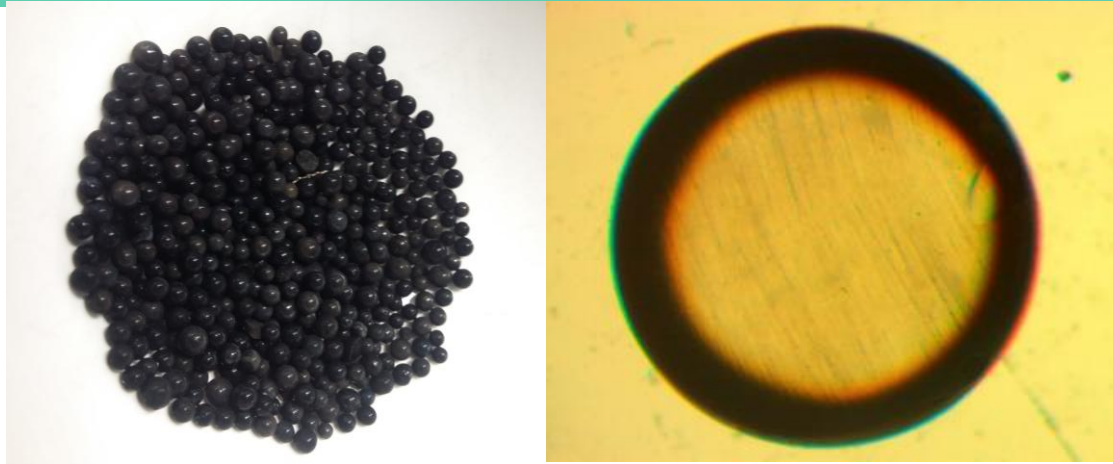
Tri-reforming of LFG

Catalyst Bed temp. (°C)	GHSV (h ⁻¹)	CH ₄ conv. (%)	CO ₂ conv. (%)	H ₂ :CO
770-810	30,000	92-99	52-72	1.70-2.23

Catalyst Optimization

- Thermally Stable
- High Surface Area
- Coke Resistant
- High OSC
- Excellent Redox Properties
- High Dispersion
- Excellent Selectivity
- High Activity
- Economical
- Low Pressure Drop



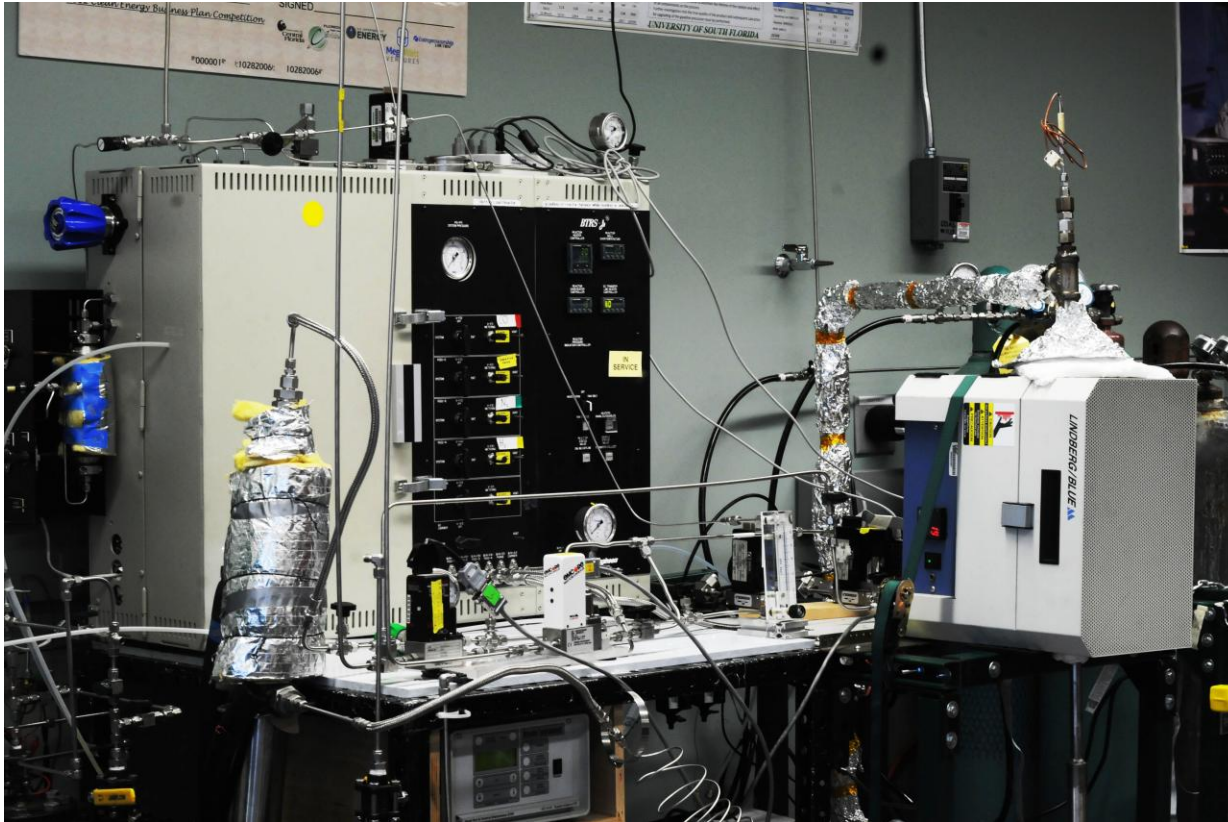


FTS Eggshell Catalyst

- Overcome mass and heat transfer limitations
- Selective product distribution in middle distillate region
- Avoid wax production

CO ₂ Conv (%)	LFG Energy Recovery In Liq Fuel (%)	Selectivity (%)		
		C ₁₋₄	CO ₂	C ₅₊
71	40	43.7	1.4	55.0

Benchscale TRIFTS Unit



- **Optimize process conditions**
- **Facilitate Pilot/Demonstration Design**
- **Plug bench data into ASPEN**
- **Update full scale techno-economic analysis**

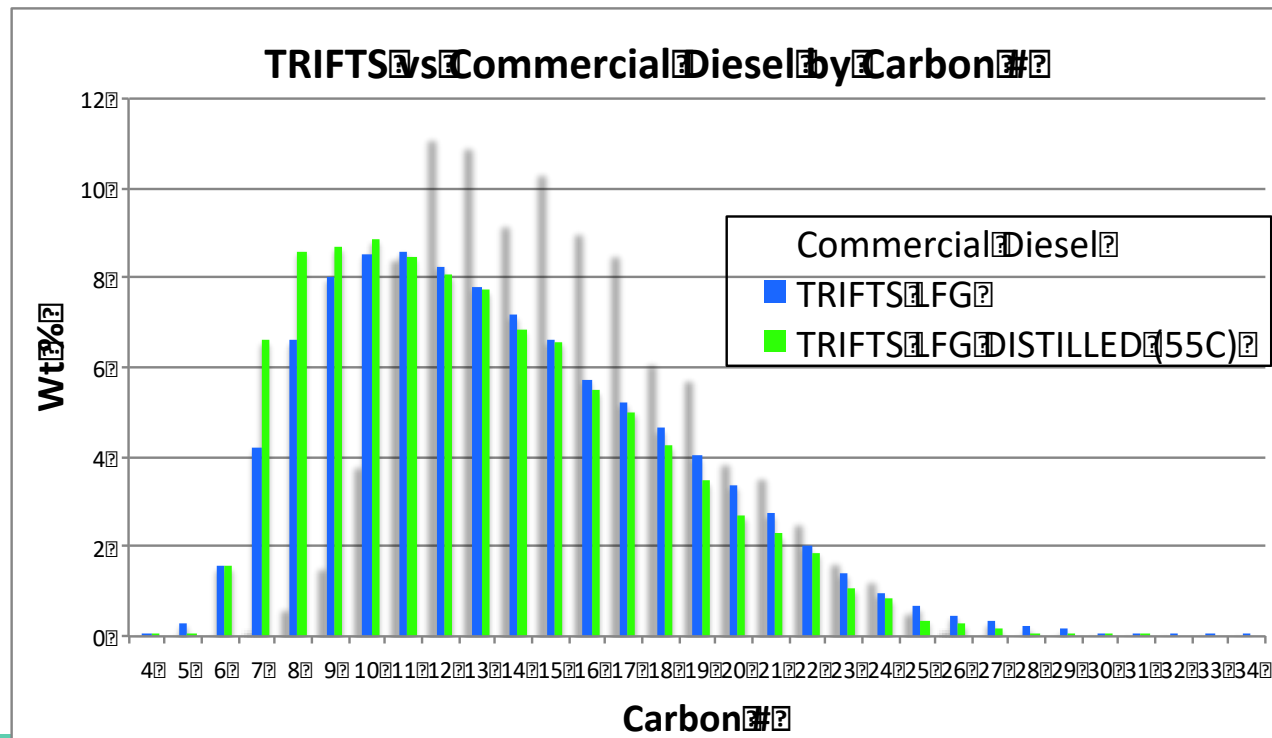
Project Overview



Fuel Analysis

- Low aromatics improve net heat of combustion and reduce soot
- Isomers improve cold temp properties
- Further reduce olefin content w/ addition of catalyst promoters
- Excellent middle distillate boiling point distribution
- Control phase separation temp to fractionate light ends
- Final boiling point aligns with commercial diesel

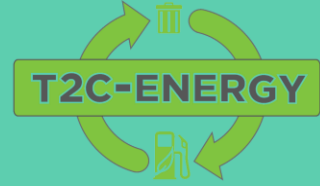
Hydrocarbon Family	T2C-E (H ₂ :CO=1.7)	Commercial Diesel
Paraffins	67.164	19.95
Isomers	28.243	31.6
Olefins	4.323	0.92
Aromatics	0.02	39.48
Cyclics	0.25	8.05



ASTM D975 “Standard Specification for Diesel Fuel Oils” Fuel Analysis Results

Fuel Analysis, ASTM Standard	Spec (No. 2 Diesel)	Commercial Diesel	TRIFTS LFG	TRIFTS LFG (Dist 5C)
Specific Gravity, ASTM D4052 (g/cc)		0.8215	0.7386	0.7489
Cetane Index, ASTM D976	≥40	57.6	84.5	72.7
Cetane Index, ASTM D4737	≥40	59.7	92.3	83.4
Flash Point, ASTM D93 (°C)	≥52	87	49	57
Cloud Point, ASTM D2500 (°C)		-6	-6	-3
Pour Point, ASTM D97 (°C)		-9	-9	-6
Distillation, ASTM D86 (°C)				
IBP: 0.5wt%		203	143	142
10%		220	164	154
50%		269	234	216
90%	282-338	329	327	314
FBP: 99.5%		378	388	378
Net Heat Comb., ASTM D3338 (MJ/kg)		43.164	44.520	44.355

Pilot/Demonstration Scale Up

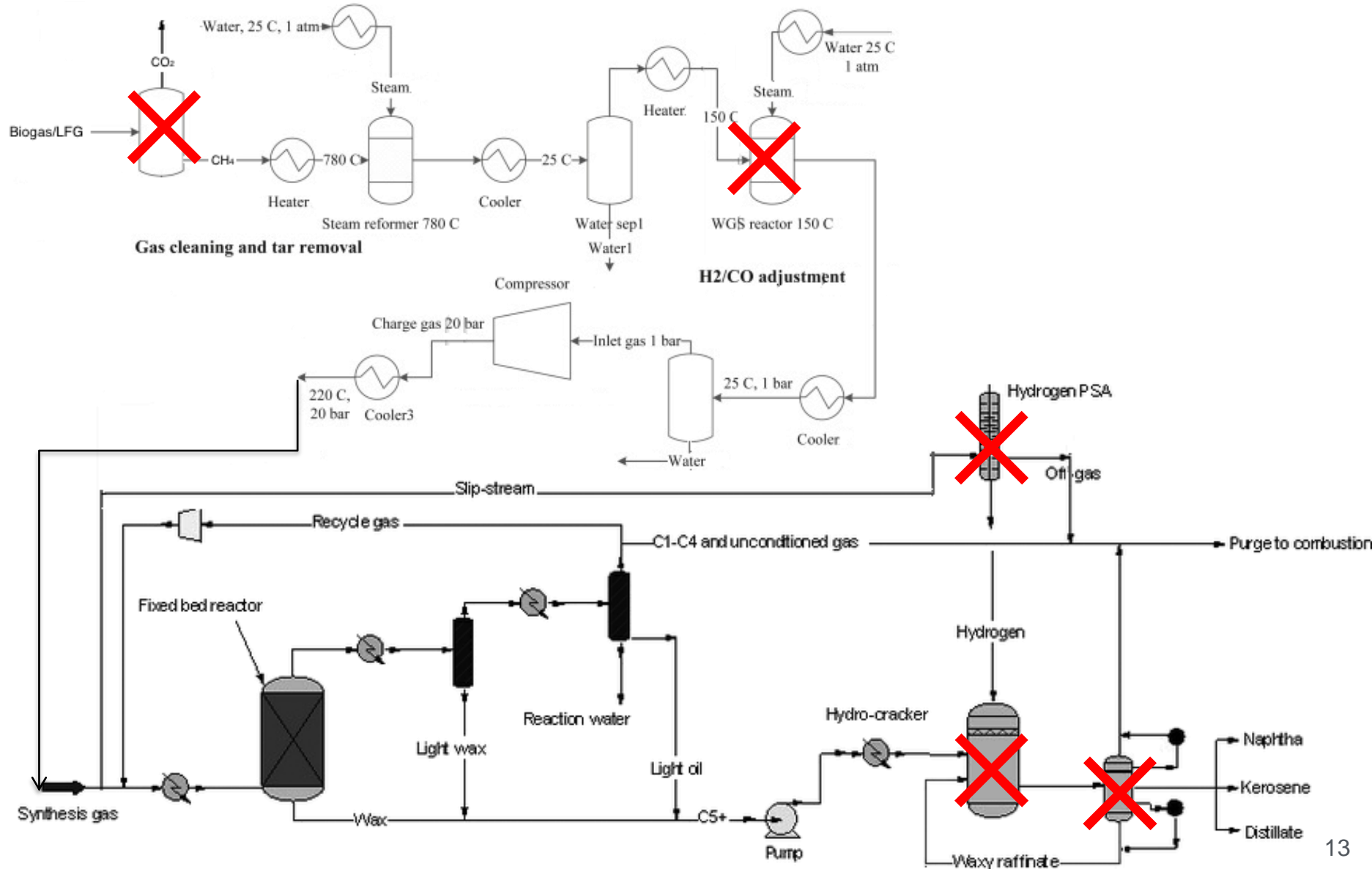


35 SCFM LFG Feed → **111 Gal/Day Diesel**

Example of skid mounted unit



Key Challenges and Approach



Key Challenges and Approach



- Reformer energy requirement met by FTS fuel gas
- Efficient heat integration
- Utility requirements provided by process itself
- Overall self sufficient process
- Minimize any outside fossil fuel derived energy inputs

Energy Requirements and Generation from 1500 scfm LFG Plant		
	BTU/hr Required	BTU/hr Produced
Reformer requires	4,472,000	
Fuel Gas Energy Content		2,488,465
Boiler	1,820,786	
LFG cooler	160,414	
Reformer HX		2,319,143
Syngas cooler	1,807,500	
FTS cooler	3,451,114	
FT reactor		9,761,143
Compressor 1	399,112	
Air Compressor 2	258,223	
Compressor 2	1,287,300	
Compressor 3	1,068,006	
TOTALS		
Equip/RXN Required	4,724,456	
Energy Produced		9,568,751
Net Energy Produced		4,844,295
Additional Electric Power Generation	0.86	MW

Scale (LFG Flowrate (SCFM))	CAPEX	Annual OPEX	Annual Revenue	Annual Profit
500	\$3.5MM	\$550k	\$3.5MM	\$2.1MM
1000	\$5.2MM	\$800k	\$7MM	\$4.5MM
1500	\$6.7MM	\$1MM	\$10.5MM	\$7.0MM
2000	\$7.9MM	\$1.2MM	\$14MM	\$9.5MM
2500	\$9.1MM	\$1.4MM	\$17.5MM	\$11MM
3000	\$10.1MM	\$1.6MM	\$21MM	\$14MM
3500	\$11MM	\$1.8MM	\$24.5MM	\$16.8MM
4000	\$11.9MM	\$2MM	\$28MM	\$19MM

Assumptions

- 15% Interest Rate
- 35% Corporate Tax
- 5.5% FCI Maintenance Budget
- 7 Full Time Staff
- Wholesale Pump Price = \$1.63
- RIN = \$4.47/gal diesel (D3 ~ \$2.63/RIN) EV=1.7

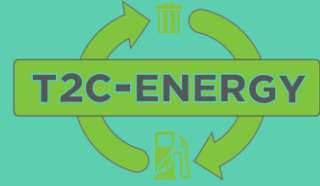
Financials (1,500 SCFM Biogas)

118 bpd (5k gal/day) Diesel Facility

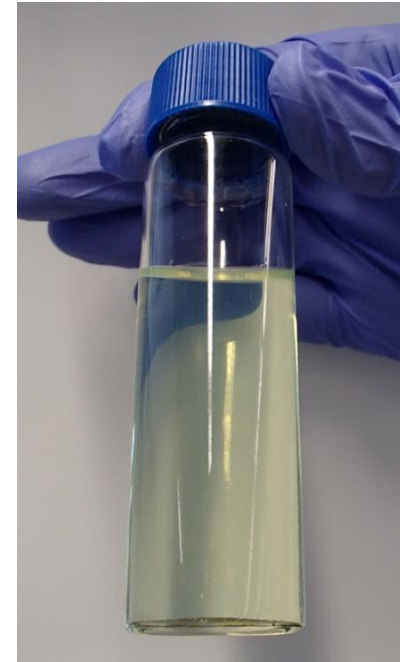


- At current WS pump price of 1.63 NPV = \$34MM
- RIN = \$4.47/gal diesel (D3 ~ \$2.63/RIN)
- Initial Construction Capital \$6.7 MM
- Breakeven No RIN credit at 900 SCFM biogas production rate

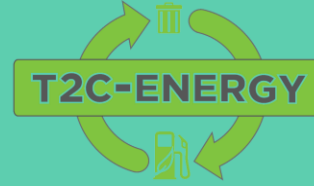
Unique Aspect Summary



- **Utilize 100% of Biogas Feedstock (CO₂ Utilization)**
- **Significant Reduction of Unit Operations**
- **Compatible with Current Infrastructure**
- **High Quality Value Add Product (Drop-In Diesel)**
- **Self Sufficient Process**
- **Produce D3/D7 RIN**
- **Vastly Improved Economics and Profitability**



Management Team



Devin Walker
CEO



Dr. John Kishner
President



Dr. Babu Joseph
VP



Timothy Roberge
CFO



Dr. Ali Gardezi
CTO

- 40+ Years in Biofuel Industry
- Recognized Industry Leaders
- Proven Track Record in Technology Scale Up
- Partnered with USCleantech and Renovare Fuels as part of US and Global Business Strategy



Sustainable Solutions for The Waste To Energy Sector